This listing of claims will replace all prior versions, and listings, of claims in the application:

LISTING OF CLAIMS:

1. **(Previously presented)** A catalyst comprising at least one ZBM-30 (molecular sieve) zeolite synthesized with a structuring agent consisting essentially of triethylenetetramine, at least one hydro-dehydrogenating element, and at least one porous mineral matrix.

2. **(Previously presented)** A catalyst according to claim 1 in which the hydro-dehydrogenating element comprises at least one of the elements of Group VIB and Group VIII of the periodic table.

3. **(Currently Amended)** A catalyst according to claim 2 in which the hydro-dehydrogenating element ~~of Group VIB~~ comprises molybdenum and/or tungsten.

4. **(Currently Amended)** A catalyst according to claim 1 in which the hydro-dehydrogenating element ~~of Group VIII~~ comprises a noble metal of Group VIII.

5. **(Currently Amended)** A catalyst according to claim 4 in which the hydro-dehydrogenating element ~~of Group VIII~~ comprises platinum and/or palladium.

6. **(Currently Amended)** A catalyst according to claim 1 wherein the catalyst has been subjected to sulphurization treatment.

7. **(Withdrawn-Currently Amended)** A process for improving the pour point of a paraffin charge, in which the charge to be treated is brought into contact with a dewaxing catalyst comprising a catalyst according to claim 1~~, at least one, element and at least one porous matrix~~.

8. **(Withdrawn-Currently Amended)** A process according to claim 7 in which the treated ~~charges contain~~ charge contains at least 20% by volume of compounds boiling above 340°C.

9. **(Withdrawn)** A process according to claim 7 in which the operating conditions are the following:

- the reaction temperature is between 200 and 450°C,
- the pressure is between 0.1 and 25 MPa,
- the hourly volume rate (hvr expressed as volume of charge injected per volume unit of catalyst per hour) is between approximately 0.05 and approximately $30h^{-1}$.

10. **(Withdrawn-Currently Amended)** A process according to claim 7 in which the charge undergoes a hydroisomerization-hydroconversion stage ~~beforehand~~ before contact with the dewaxing catalyst.

11. **(Withdrawn-Currently Amended)** A process according to claim 10 in which all of the effluent from the hydroisomerization-conversion stage is ~~sent to~~ contacted with the dewaxing catalyst.

12. **(Withdrawn)** A process according to claim 10 in which the hydroisomerization-hydroconversion stage is preceded by a hydrorefining stage.

13. **(Withdrawn-Currently Amended)** A process according to claim 12 in which the hydrorefining stage is followed by an intermediate separation before the hydroisomerization-hydroconversion stage.

14. **(Withdrawn-Currently Amended)** A process according to claim 7 in which the effluent from the ~~catalytic hydrodewaxing stage~~ contacting with a dewaxing catalyst step is at least partly sent to contact with a hydrofinishing catalyst.

15. **(Previously presented)** A catalyst according to claim 1, wherein the at least one porous mineral matrix is an amorphous or poorly crystallizable oxide.

16. **(Previously presented)** A catalyst according to claim 1, wherein the hydro-dehydrogenating agent comprises platinum and the at least one porous mineral matrix comprises alumina.